



SOLID PARTICLE EROSION IN THE SUDDEN CONTRACTION OF RAW WATER PIPELINE

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Abstract

The steady 3-D raw water turbulent flow is numerically investigated. This flow is formed of solid silica sand (quartz) carried by water in stainless steel pipe. The flow in a straight pipe and flow in a pipe with a sudden contraction are analyzed using a two-way coupled Eulerian-Lagrangian approach. Erosion rate is estimated by Oka erosion model combined with the constant coefficient of restitution. The effect of solid particles mass flow rate, inlet velocity, particle diameter, internal pipe diameter, orientation, contraction coefficient, and wall pipe contraction angle on erosion rate are examined. The predicted erosion is distributed homogeneously for straight pipe, while the step wall area of the contraction is the most eroded part. The erosion rate increases with the increase of solid particles diameter, flow rate, inlet velocity, and decreasing pipe diameter. It is found that the erosion is limited till the particle diameter reaches 500 μm then it starts to increase. The erosion rate increases with decreasing contraction coefficient and step wall angle. When the step wall angle decreased to 300, the erosion rate is reduced by 30 times that for 900. So, decreasing step wall angle can be considered as a geometrical solution to reduce erosion rate.

Keywords: (erosion, solid particle, CFD, model calculation, pipe contraction)

1. INTRODUCTION

Erosion due to solid particle impact is the most serious problem that occurs in piping fittings in different industrial applications such as: oil and gas production, water filtration stations, turbines, pumps etc. The erosion causes serious problems such as: leakage, vibration, energy losses, a complete failure of the turbomachine and economic loss. Studying solid particle erosion in multiphase flow still remains a challenging area for researches, since predicting the motion of particles before and after impaction and knowing impaction properties in turbulent flow as well as the effect of forces acting on particle by the fluid itself are not an easy task.

Many previously studies related to the erosion in pipe and pipes fittings due to fluid-solid flow are found. Al-Baghdadi et al. [2] developed a 3-D Computational Fluid Dynamics (CFD) model to describe the turbulent transport of sand particles and crude oil through elbows to estimate erosion rate. Al-Khayat et al. [3] studied the erosion due to 3-D flow of crude oil in elbow using CFD. The friction forces between crude oil or sand particles and pipe wall, fluid viscosity, temperature, density and mass flow rate has been studied in the model and well agreed with previously published results. Ataiwi et al. [5] and Yousif et al. [43] studied experimentally the effect of particle size, impingement angle and the

effect of using mixed grain size of particles rather than using only one size on erosion rate. Clark [6] illustrated that the solid particle erosion depends on particle properties, metallic properties, geometry, type of flow and flow pattern. The erosion mechanism in both ductile and brittle materials was extensively studied by Finnie [8,9], Jordan [15], Hutchings and Winter [11], Leavy [18], Mansouri [20] and others. For ductile material, the erosion occurs by scraping mechanism or plastic deformation mechanism. The erosion in brittle material is widely understood, which occurs by formation and propagation of cracks by chipping mechanism or cracking mechanism. The influence of wall roughness on erosion rate in gas-solid turbulent annular pipe flow was numerically studied by Jafri et al. [12]. The effect of impingement angle, velocity, particle size and concentration on erosion rate in slurry flow was experimentally investigated by Jha et al. [13] and Patil et al. [31]. An experimental and CFD erosion modelling of large radius pipe elbows with solid-liquid flow is presented by Johar et al. [14]. Kang et al. [16] presented an integral model for predicting sand erosion in elbow for gas-liquid multiphase flow, the effect of flow pattern (bubble flow, slug flow, churn flow and annular flow) on erosion rate has been examined. The erosion model also validated with 108 experiments and reported a good matching.

Other researches are studied the solid particle erosion in other complex geometries. Kosinska et al. [17] analyzed theoretically the erosion due to the simulated fluid flow laden with nano and micro sized particles in pipe elbow, the results are validated with experiments and they were coincided. Mazumdar et al. [21] measured the particle impact velocity that cause erosion wear in solid-liquid flow in elbow numerically and experimentally. The numerical study is presented by using discrete phase model (DPM) with erosion/accretion model in the commercial CFD Fluent software. The experimental study is presented using Particle Image Velocimetry (PIV) technique. The numerical and experimental studies showed a good agreement. The effect of elbow radius on pressure drop in multiphase flow was also numerically investigated [22]. Mazumder [23] simulated the effect of fluid-solid flow velocity, particle size and type of fluid on the location and magnitude of maximum erosion in U bend. Meng and Ludema [24] presented erosion models previously developed and the parameters that affect the erosion rate. They found that there are 28 erosion models related with solid particle erosion and 33 parameters affect the erosion. Parsi et al. [30] investigated experimentally the effect of flow pattern and flow orientation on erosion caused by sand particles in elbows with gas-liquid-solid multiphase flow condition. Ultrasonic Technique (UT) is used to measure erosion rate and the technique of Wire Mesh Sensor (WMS) is used to study flow pattern and their effects on erosion. Peng and Cao [32] performed a numerical simulation to study solid particle erosion in a pipe bend for solid-liquid flow. The effect of Stokes number, bend orientation and flow direction on the maximum erosion rate was also studied. Peng et al. [33] studied numerically and experimentally the erosion by sand entrained in slug flow in a horizontal pipe bend. The experimental study applied by designing a flow loop with a detachable test pipe bend and the numerical study applied by Volume Of Fluid model (VOF) and Discrete Phase Model (DPM) model in the commercial CFD Fluent code. Raghavendra et al. [35] presented a CFD simulation of erosion wear by sand-water flow in choke valves. The net eroded surface was measured by using modern technique which is Coordinate Measurement Machine (CMM). Shamshirband et al. [38] presented a performance investigation of micro and nano sized particles caused erosion in elbow using adaptive Neuro-Fuzzy Interface System (ANFIS) model. Vieira et al. [41] measured elbow solid particle erosion in multiphase annular flow by using an electrical resistance probe. Other parameters are also examined such as: particle size, fluid viscosity, liquid flow rate, orientation and location of probe. Zhang et al. [44] studied the erosion caused by solid-gas flow in a model of break valve.

It is clear that the erosion of simple piping geometries such as straight pipe and pipe bend is studied in the most of the previous studies. While, a

rare erosion investigation in the more complex piping fittings is available. The objectives of this work are: first, to conduct a parametric study of the solid particle erosion using CFD technique on flow through more complex piping geometries such as: pipe with sudden contraction. Second, study the effects of some parameters that related to sand-water two phase turbulent flow with erosion. Third, to propose a geometrical solution to reduce erosion rate.

2. MATHEMATICAL MODEL

In this work, three mathematical models namely: flow modelling, particle tracking and erosion prediction are utilized to study solid particle erosion problem.

2.1. Flow modelling

The Eulerian-Lagrangian approach is used to model the solid-liquid flow by solving Reynolds Averaged Navier-Stock's equations (RANS) in Eulerian scheme. While, the particles are treated as discrete phase. The trajectories of solid particles are computed by solving the equation of motion of particles through using Discrete Phase Model (DPM) in Lagrangian scheme [1]. The Eulerian-Lagrangian approach is only applicable when the volume fraction of solid particles is low comparing with that of fluid phase. Because, with increasing particles, the computational time increased and simulation quality reduced and the particles trajectories are required to solve for each parcel [39]. The volume fraction of solid particles should not exceed 10% - 12% to be able to use DPM model and the particles are diluted in the fluid phase [4]. A Newtonian incompressible three-dimensional (3-D) fluid flow with constant thermophysical properties are considered in this work. The governing differential equations for continuity and momentum are: [4, 42]

$$\frac{\partial \rho}{\partial t} + \vec{\nabla} \cdot (\rho \vec{v}) = 0 \quad (1)$$

$$\frac{\partial}{\partial t} (\rho \vec{v}) + \vec{\nabla} \cdot (\rho \vec{v} \vec{v}) = -\vec{\nabla} p + \vec{\nabla} \cdot [\mu ((\nabla \vec{v} + \nabla \vec{v}_t))] + \rho \vec{g} + \vec{S}_M \quad (2)$$

where:

\vec{v} is the fluid velocity vector in the cylindrical coordinate system (m/s), which is defined:

$$\vec{v} = v_r \hat{r} + v_\theta \hat{\theta} + v_z \hat{z} \quad (3)$$

where:

\hat{r} , $\hat{\theta}$ and \hat{z} are unit vectors in the r , θ , and z directions respectively.

v_r , v_θ , and v_z are the velocity components (m/s) in the r , θ and z directions respectively.

$\vec{\nabla}$ is the dell operator vector (gradient operator) which is defined as:

$$\vec{\nabla} = \frac{\partial}{\partial r} \hat{r} + \frac{\partial}{\partial \theta} \hat{\theta} + \frac{\partial}{\partial z} \hat{z} \quad (4)$$

ρ is the fluid density (kg/m^3).

p is the pressure (Pa).

\vec{g} is the gravitational acceleration (m/s^2).

μ is the dynamic viscosity of the fluid (kg/m.s).

v_t is the fluctuated velocity due to turbulence (m/s). S_m is the momentum transfer between fluid phase and solid particle phase ($\text{kg/m}^2 \cdot \text{s}^2$).

2.1.1. Turbulence model

The standard k- ε turbulence model is adopted to resolve flow turbulence. The model is chosen because of its' computational efficiency and its' simplicity [37]. The flow is assumed as a fully turbulent and the effects of molecular viscosity are neglected [4]. The standard k- ε model is semi-empirical model which consists of the turbulent kinetic energy (k) equation and the dissipation rate of turbulent kinetic energy (ε) equation such that:

$$\frac{\partial}{\partial t}(\rho k) + \nabla \cdot (\rho \vec{v} k) = \nabla \cdot \left[\left(\mu + \frac{\mu_t}{\sigma_k} \right) \nabla k \right] + G_K - \rho \varepsilon + S_K \quad (5)$$

$$\frac{\partial}{\partial t}(\rho \varepsilon) + \nabla \cdot (\rho \vec{v} \varepsilon) = \nabla \cdot \left[\left(\mu + \frac{\mu_t}{\sigma_\varepsilon} \right) \nabla \varepsilon \right] + \frac{\varepsilon}{k} (C_{\varepsilon 1} G_K - \rho \varepsilon C_{\varepsilon 2}) + S_\varepsilon \quad (6)$$

where:

k is the turbulence kinetic energy (m^2/s^2).

ε is the dissipation in the turbulent kinetic energy (m^2/s^3).

μ_t is the turbulent (or eddy) viscosity ($\text{kg/m} \cdot \text{s}$), which is obtained as:

$$\mu_t = \rho C_\mu \frac{k^2}{\varepsilon} \quad (7)$$

σ_k is the turbulent Prandtl number for k which equal to (1.0).

σ_ε is the turbulent Prandtl number for ε which equal to (1.3).

G_K is the generation of turbulent kinetic energy due to the mean velocity gradient ($\text{kg/m} \cdot \text{s}^3$). It is obtained as: [30]

$$G_K = \mu_t \nabla \vec{v} \cdot (\nabla \vec{v} + \nabla \vec{v}_t) - \frac{2}{3} \nabla \cdot \vec{v} (3\mu_t \nabla \cdot \vec{v} + \rho k) \quad (8)$$

$C_{\varepsilon 1}$, $C_{\varepsilon 2}$ and C_μ are constants and equal to 1.44, 1.92 and 0.09 respectively.

S_K is the source term for turbulent kinetic energy ($\text{kg/m} \cdot \text{s}^3$).

S_ε is the source term for the dissipation rate of turbulent kinetic energy ($\text{kg/m} \cdot \text{s}^4$).

2.2. Particle tracking

The Lagrangian scheme is adopted to track the solid particles trajectories in the flow by solving particle's equation of motion (Newton's equation of motion). The software integrates the force balance for particle to find the particle trajectory and this force balance equals the particle inertia with forces acting on the particle and this is called "Discrete Phase Model" (DPM) [1]. Particle tracking is based on assuming constant thermophysical properties for solid particles. The particles injected with the same fluid velocity at pipe inlet. The particle is carried out by the fluid and no particle-particle interaction occurs. The particle has a semi-round shape and it would not deform or break during collision. The particle's equation of motion is: [42]

$$m \frac{d\vec{v}_p}{dt} = \sum F = \vec{F}_D + \vec{F}_P + \vec{F}_{VM} + \vec{F}_G + \vec{F}_B \quad (9)$$

where:

\vec{v}_p is the particle velocity vector in the cylindrical coordinate system (m/s) which is defined:

$$\vec{v}_p = v_{pr} \hat{r} + v_{p\theta} \hat{\theta} + v_{pz} \hat{z} \quad (10)$$

in which, v_{pr} , $v_{p\theta}$ and v_{pz} are the particle velocity components in the r , θ and z directions respectively.

m is particle mass (kg).

F_D is the drag force (N).

F_P is the pressure gradient force (N).

F_{VM} is the virtual mass force (N).

F_G is the gradient gravity force (N).

F_B is the buoyancy force (N).

The Magnus, Basset and Shaffman lift forces are neglected because they are too small comparing with other acting forces when the carrier fluid is water [4].

The drag force is defined as:

$$\vec{F}_D = C_D \rho \frac{\pi d_p^3}{8} |\vec{v} - \vec{v}_p| (\vec{v} - \vec{v}_p) \quad (11)$$

where:

d_p is the particle diameter (m).

C_D is the drag coefficient.

Several drag laws are available in Eulerian-Lagrangian model. In this study, the spherical drag law is used:

$$C_D = a_1 + \frac{a_2}{Re_p} + \frac{a_3}{Re_p^2} \quad (12)$$

where:

Re_p is the particle relative Reynolds number.

The constants a_1 , a_2 and a_3 are obtained according to the particle relative Reynolds number (Re_p) as given in Table (1) [25]:

Table 1. Drag coefficients [34]

Reynolds range	a_1	a_2	a_3
$Re_p < 0.1$	0	24.0	0
$0.1 < Re_p < 1.0$	3.69	22.73	0.0903
$1.0 < Re_p < 10.0$	1.222	29.1667	-3.8889
$10.0 < Re_p < 100$	0.6167	46.5	-116.67
$100 < Re_p < 1000$	0.3644	98.33	-2778
$10^3 < Re_p < 5 \cdot 10^3$	0.357	148.62	-4.755×10^4
$5 \cdot 10^3 < Re_p < 10^4$	0.46	-490.546	5.787×10^5
$10^4 < Re_p < 5 \cdot 10^4$	0.5191	-1662.5	5.4167×10^6

$$Re_p = \rho \frac{|\vec{v} - \vec{v}_p|}{\mu} d_p \quad (13)$$

The buoyancy and gravity forces are combined together such that:

$$\vec{F}_B = (\rho_p - \rho) \vec{g} \frac{\pi d_p^3}{6} \quad (14)$$

In which ρ_p is the density of solid particles (kg/m^3).

The virtual mass force is defined as:

$$\vec{F}_{VM} = \frac{\pi d_p^3}{12} \rho \frac{d}{dt} (\vec{v} - \vec{v}_p) \quad (15)$$

The pressure gradient force is expressed as:

$$\vec{F}_P = \rho \frac{\pi d_p^3}{6} \vec{v}_p \nabla \vec{v} \quad (16)$$

2.2.1. Coupling between two phases

The coupling (interaction) between solid phase and the fluid phase is expressed by the momentum exchanged between the two phases, that is called

"coupling". In this study, the two-way coupling is adopted i.e the carrier fluid influences the solid particles via drag and turbulence, and the solid particles turn influence via turbulence and reduction in momentum. The interaction between phases is done through the source terms: (S_M) in equation (2), (S_k) in equation (5) and (S_ε) in equation (6), in which these effects are considered [32].

2.2.1.1. Momentum coupling

The momentum exchanged between the two phases is computed by examine the momentum changing in particle for each control volume. The momentum changing is computed as: [4,32]

$$S_M = \sum(F_D + F_P + F_{VM} + F_B)m_p \Delta t \quad (17)$$

Where, m_p is the mass flow rate of solid particles (kg/s), and Δt is the time step (s).

2.2.1.2. Turbulence coupling

Fluid velocity is formed of mean and random fluctuated velocity, such as:

$$v_r = \bar{v}_r + v'_r \quad (18)$$

$$v_\theta = \bar{v}_\theta + v'_\theta \quad (19)$$

$$v_z = \bar{v}_z + v'_z \quad (20)$$

where:

\bar{v}_r , \bar{v}_θ and \bar{v}_z are the mean fluid velocity in the r , θ and z directions respectively.

v'_r , v'_θ and v'_z are the random fluctuated velocity in the r , θ and z directions respectively.

The random fluctuated velocity (v'_r , v'_θ and v'_z) influences the particles trajectories. In this work, the particle-eddy interaction model proposed by Gosman and Ioannides [10] is adopted. The effect of turbulence on solid particles is considered by using Discrete Random Walk (DRW) model, or (eddy life) model. In which, each eddy is characterized by the Gaussian distributed of random fluctuation velocity v'_r , v'_θ and v'_z : [4, 32]

$$v'_r = \zeta \sqrt{v_r'^2} \quad (21)$$

$$v'_\theta = \zeta \sqrt{v_\theta'^2} \quad (22)$$

$$v'_z = \zeta \sqrt{v_z'^2} \quad (23)$$

where:

ζ is the random number that obeys normal distribution and the right-hand side terms represent the local Root-Mean-Square (RMS) value of the velocity fluctuation.

The two-way coupling enables to consider the effects of changing turbulence quantities due to particle damping and turbulence eddies by modification the source terms (S_k) and (S_ε) in the standard k- ε model by the formulation described in [7].

2.2.2. Particle impact and rebound behaviour

When solid particle collides the wall, some of its' energy will lose and the rebounded velocity after impaction will be less than the incident velocity before impaction [32]. The coefficient of restitution

is defined as the ratio of the post-collision and pre-collision velocities which consists of two components, one acts along the normal and the other acts along the tangential of the wall [21]. According to [36], the average coefficient of restitution for quartz sand particles collide with stainless steel material is 0.68.

2.3. Erosion prediction

In this work, the Oka erosion model is adopted since it is related with the most effective parameters on erosion such as: particles' diameter, impact angle, velocities and material properties for particles and target material. The thermophysical properties for wall material are considered constant and the deformation of wall material due to solid particles collision is ignored in this model. The erosion rate according to [3,32] is expressed as:

$$ER = 1.0 \times 10^{-9} \rho_w k f(\alpha) (H_v)^{k1} \left(\frac{v_p}{v^*}\right)^{k2} \quad (24)$$

$$f(\alpha) = (\sin \alpha)^{n1} [1 + H_v(1 - \sin \alpha)]^{n2} \quad (25)$$

where:

ρ_w is the density of target material (kg/m³).

H_v is Vickers hardness of target material (GPa).

α is the impact angle between solid particle and target material (degree).

v^* is the reference velocity of solid particle (m/s).

d^* is the reference particle diameter (μm).

k , $k1$, $k2$, $k3$, $n1$ and $n2$ are constants, their values are given in Table (2).

Table 2. The values of constants parameters in Oka erosion model [28]

k	$k1$	$k2$	$k3$
65	-0.12	$2.3(H_v)^{0.038}$	0.19
$n1$	$n2$	$v^*(\text{m/s})$	$d^*(\mu\text{m})$
$0.71(H_v)^{0.14}$	$2.4(H_v)^{-0.94}$	104	326

The stainless steel 304H (SS304H) has been chosen to be the main material of the piping wall, since it has a high resistance of corrosion [19]. The solid particles have been chosen to be silica sand (quartz) and the carrier fluid is the water. The physical properties of SS304H, quartz sand and water are listed in Table (3).

Table 3. Physical properties for SS304H, Quartz sand and water [27, 28 and 45]

Stainless steel 304H (SS304H)	
Density (kg/m ³)	7890
Young modules (MPa)	1.948×10^5
Poisson ratio	0.27
Vickers hardness (GPa)	1.8
Internal diameter (m)	0.4064
Quartz sand	
Density (kg/m ³)	2600
Young modules (MPa)	370
Poisson ratio	0.3
Diameter (m)	4×10^{-4}
Water	
Density (kg/m ³)	998.2
Dynamic viscosity (pa s)	1.003×10^{-3}

3. COMPUTATIONAL ANALYSES

3.1. Physical and computational domain

ANSYS-Fluent 2020 R2 Computational Fluid Dynamics (CFD) software is used to simulate solid particle erosion for sand-water two-phase 3-D flow through two piping geometries namely: straight pipe and pipe with sudden contraction as presented in Fig. (1). The internal diameter for the straight pipe is 406.4 mm (16 inch) with 8128 mm length. While, the pipe with sudden contraction has internal diameters of 406.4 mm for the larger section and 300 mm for the smaller section with 4064 mm length for each part. The pipe wall material is SS304H with the physical properties given in Table (3). The established assumptions are: Steady turbulent 3-D flow, Newtonian incompressible fluid, constant thermophysical properties, the solid particles are at the same fluid velocity at the pipe inlet, no particle-particle interaction occurs. The Magnus, Basset and Shaffman lift forces on particle are neglected. The particles have a semi-round shape and they would not deform or break during collision and the wall deformation caused by particles collision is not considered.

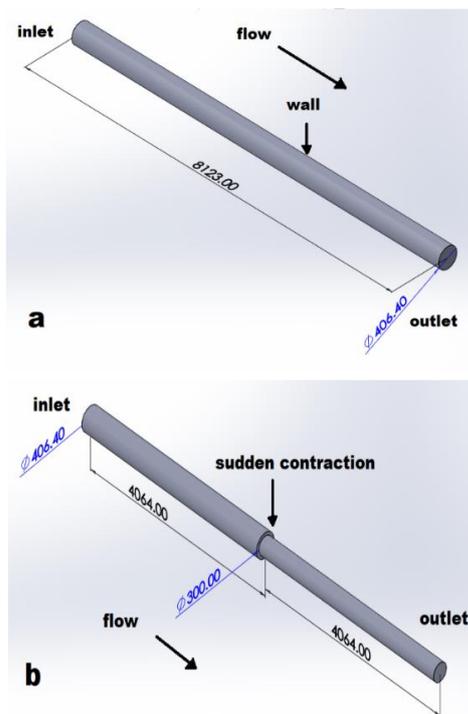


Fig. 1. (a) Straight Pipe (b) Pipe with Sudden Contraction

Table 4. Boundary conditions for continuous phase and dispersed phase

Continues Phase		Dispersed Phase	
Inlet	Constant Velocity	Inlet	"Escape"
Outlet	Constant Pressure	Outlet	"Escape"
Wall	No-Slip Condition	Wall	"Reflect"

The boundary conditions for the continuous phase (water) and dispersed phase (sand particles) are listed in Table (4).

3.2. Grid generation

ANSYS ICEM CFD software is adopted to generate hexahedral mesh to guarantee more stability and generate fewer highly distorted elements for three dimensional piping geometries as presented in Fig. (2). Also the computational accuracy of hexahedral elements is higher than the tetrahedral one. Near wall finer grid is generated to capture the boundary layer as illustrated in the zoomed section in Fig. (2).

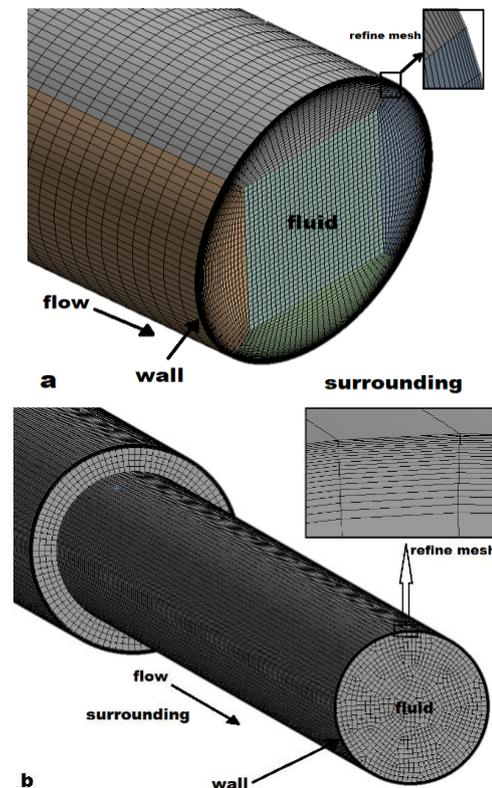


Fig. 2. The hexahedral mesh in (a) straight pipe (b) pipe with sudden contraction

Grid independency is accomplished by solving water flow (single phase) to compute water velocity at different sections in each geometry. The middle and outlet sections for straight pipe are selected. While, for the pipe with sudden contraction, the middle and outlet sections for small pipe diameter are checked. It is showed that the best mesh density for straight pipe and for pipe with sudden contraction is 717120 and 629620 hexahedral cells respectively as shown in Fig.s (3) and (4).

3.3. Numerical scheme

The numerical scheme settings for water-sand two-phase flow through straight pipe and pipe with sudden contraction are given in Table (5). For the convergence and stability of solution, appropriate setting values of under-relaxation factors and residual should be selected. The values of under-

relaxation factors are given in Table (6). The maximum residual value for all parameters has been set as default to be 0.001.

The numerical simulation of water-sand two-phase flow through two piping geometries is performed according to the flow conditions given in Table (7).

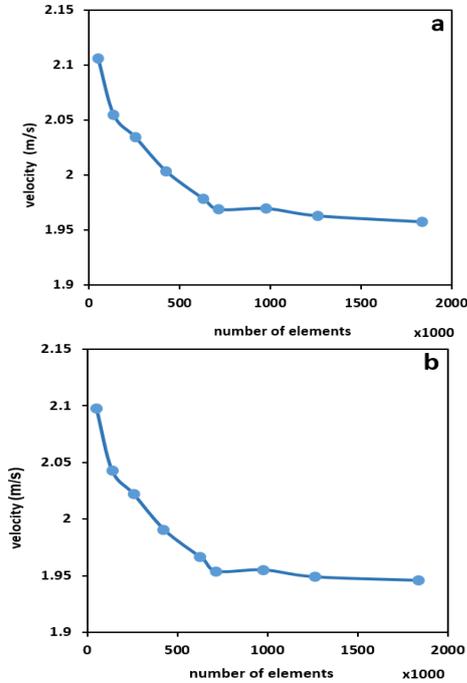


Fig. 3. Grid independency for straight pipe case at: (a) middle section (b) outlet section

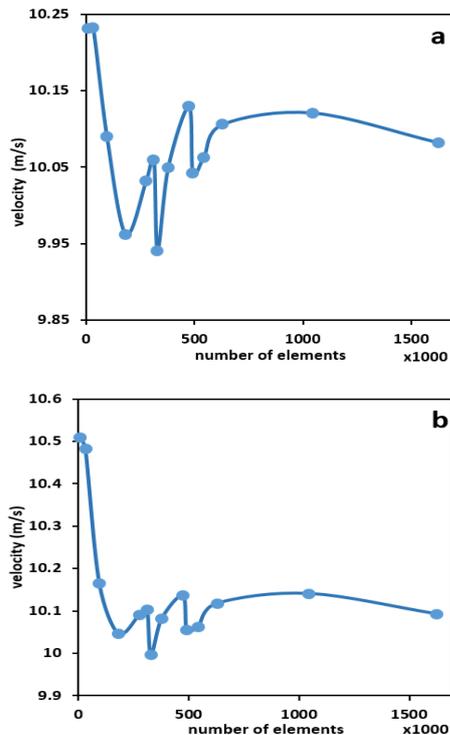


Fig. 4. Grid independency for pipe with sudden contraction case at: (a) middle section of small pipe (b) outlet section of small pipe

3.4. Validation of the model

The present computational results are verified with the experimental results by Postlethwaite and Nestic [34]. They measured the erosion rate for slurry flow (water-silica sand flow) through sudden contraction, groove and sudden expansion, as shown in Fig. (5). The experimental parameters and flow condition of the study are given in Table (8).

Table 5. Numerical Scheme

Variable	Sittings
Solver type	Pressure-based solver
Pressure-velocity coupling	SIMPLIC algorithm
Pressure spatial discretization	Second order
Momentum spatial discretization	Second order upwind
Turbulent kinetic energy spatial discretization	Second order upwind
Turbulent dissipation rate spatial discretization	Second order upwind
Turbulence model	Standard k-ε model
Near wall treatment	Scalable wall function
Particle treatment	Discrete Phase Model (DPM)
Particle tacking scheme	Trapezoidal
Interaction between phases	Two-way coupling
Erosion estimation	Oka erosion model

Table 6. Under-Relaxation Factors

Parameters	Value
Pressure	0.3
Density	1
Body forces	1
Momentum	0.7
Turbulent kinetic energy	0.8
Turbulent dissipation rate	0.8
Turbulent viscosity	1
Discrete phase sources	0.5

Table 7. Flow conditions of the numerical simulation

Parameter	Values
Carrier fluid	water
Solid particles	Quartz sand
Piping wall material	Stainless steel 304H
Mass flow rate for particles (kg/s)	(1, 5, 10, 50 and 100) × 10 ⁻³
Inlet velocity (m.s)	6, 7, 8, 9 and 10
Particle size (μm)	400, 450, 500, 550 and 600
Pipe diameter (mm)	406.4, 350, 300, 250 and 203.2
Orientation	Horizontal and vertical
Contraction coefficient in pipe with sudden contraction	0.741, 0.544, 0.378, 0.25 and 0.136
Step wall angle of the contraction	90°, 75°, 60°, 45° and 30°

To validate the erosion in straight pipe and in pipe with sudden contraction, section 1 and section 2 in Fig. (5) is simulated with the flow conditions given in Table (8) respectively. The validation of straight pipe case (section 1) showed a good agreement with experiments with a percentage deviation of 7.6%. Where, the maximum erosion from experiments is (7.57 mm/year) and from numerical simulation is (7 mm/year) as shown in Fig. (6). Also, the validation of pipe with sudden contraction (section 2) showed an acceptable agreement with experiments with 11% deviation. In which, the maximum erosion from experiments is (137 mm/year) and from numerical simulation is (121.9 mm/year) as shown in Fig. (6).

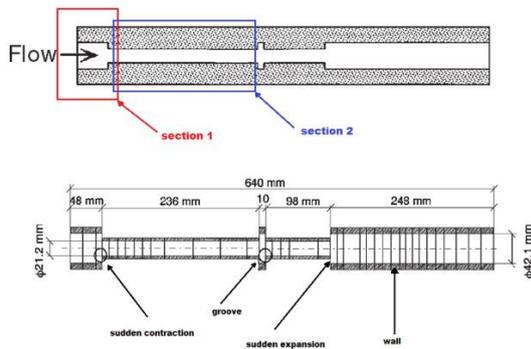


Fig. 5. The complex piping geometry for experimental study of Postlethwaite and Nestic [34]

Table 8. Experimental parameters and flow conditions

Carrier fluid	Water, 995.6 (kg/m ³) density, 7.97 × 10 ⁻⁴ (pa.s) viscosity
Pipe material	Stainless steel 304 (UNS S30400)
Solid particles	Silica sand particles
Internal pipe diameter	42.1 (mm) for large pipe, 21.2 (mm) for small pipe
Flow velocity	3.3 (m/s) for large pipe, 13.3 (m/s) for small pipe
Particles mass flow rate	0.294 (kg/s)
Particle average diameter	430 (μm)

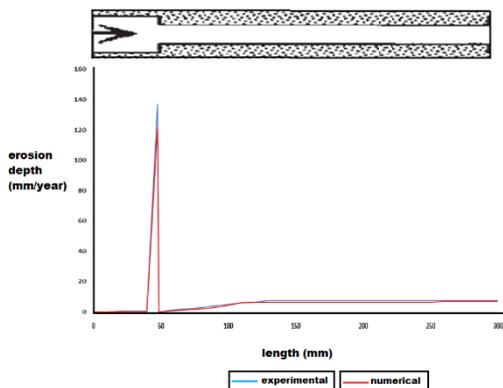


Fig. 6. Comparison of erosion depth profile between numerical results and experimental data of Postlethwaite and Nestic [34]

4. RESULTS AND DISCUSSION

4.1. Straight pipe case

The fluid velocity and streamlines distribution didn't change along the straight pipe because there is no changing in flow direction or cross section as shown in Fig. (7). The sand particles affected by the turbulence of flow and by the forces acting on, which leads to collide with wall and cause homogenous erosion along the pipe by (8.72 × 10⁻¹¹ kg/m².s) as shown in Fig.(8). The effect of mass flow rate of sand particles, inlet flow velocity, particle diameter and internal pipe diameter on erosion has been illustrated in Table (9).

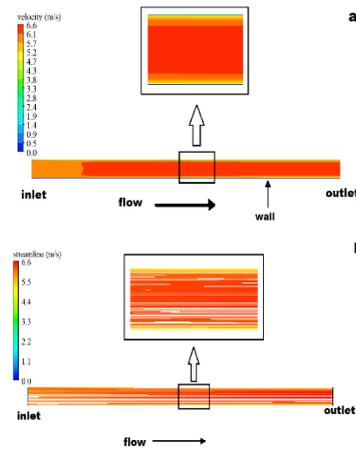


Fig. 7. Distribution of (a) velocity (b) streamlines

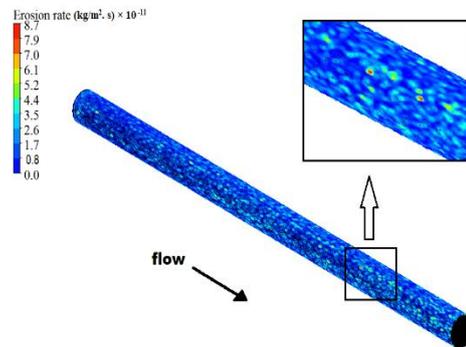


Fig. 8. Erosion behavior in straight pipe case

4.1.1. Effect of mass flow rate of sand particles

The erosion rate is increased with increasing mass flow rate of sand particles as given in Table (9). The investigated mass flow rates are: 0.001, 0.005, 0.01, 0.05 and 0.1 kg/s .The erosion rate is increased with mass flow rate, it was (8.72 × 10⁻¹¹ kg/m².s) for 0.001 kg/s and increased to (9.83 × 10⁻⁹ kg/m².s) i.e by 111.7% when mass flow rate increased to 0.1 kg/s as given in Table (9). This increase of erosion rate is reported since more particles collide with pipe wall material leads to more erosion. Fig. (9-a) showed the relationship between mass flow rate and erosion rate in straight pipe.

Table 9. The effects of different parameters on erosion rate in straight pipe case I

Mass flow rate of particle (kg/s)	Inlet velocity of fluid (m/s)	Particle diameter (μm)	Internal pipe diameter (mm)	Erosion rate $\text{kg/m}^2 \cdot \text{s}$
0.001	6	400	406.4	8.72×10^{-11}
0.005	6	400	406.4	4.67×10^{-10}
0.01	6	400	406.4	1.53×10^{-9}
0.05	6	400	406.4	7.05×10^{-9}
0.1	6	400	406.4	9.83×10^{-9}
0.001	7	400	406.4	1.19×10^{-10}
0.001	8	400	406.4	1.79×10^{-10}
0.001	9	400	406.4	1.98×10^{-10}
0.001	10	400	406.4	2.70×10^{-10}
0.001	6	450	406.4	9.50×10^{-11}
0.001	6	500	406.4	1.03×10^{-10}
0.001	6	550	406.4	3.67×10^{-10}
0.001	6	600	406.4	5.12×10^{-10}
0.001	6	400	350	1.13×10^{-10}
0.001	6	400	300	1.41×10^{-10}
0.001	6	400	250	2.53×10^{-10}
0.001	6	400	203.2	3.27×10^{-10}

4.1.2. Effect of inlet flow velocity

In this work five fluid inlet velocities are investigated: 6, 7, 8, 9 and 10 m/s. Fig. (9-b) shows that erosion rate is increased with increasing flow velocity as given in Table (9). It was ($8.72 \times 10^{-11} \text{ kg/m}^2 \cdot \text{s}$) at 6 m/s inlet velocity, then increased by 36.5% when inlet velocity increased by 16.7% i.e ($1.19 \times 10^{-10} \text{ kg/m}^2 \cdot \text{s}$). The erosion rate increase reaches 210% at 10 m/s inlet velocity. The erosion rate rising occurs due to the increase in particle speed i.e increase of particle momentum leading to increase impaction energy and more erosion in pipe wall material.

4.1.3. Effect of particle diameter

The erosion rate in straight pipe is increased as particle diameter increased as illustrated in Fig. (9-c) and given in table (9). Five particle diameters have been examined: 400, 450, 500, 550 and 600 μm . It is reported that the erosion rate was ($9.5 \times 10^{-11} \text{ kg/m}^2 \cdot \text{s}$) at 450 μm). The erosion rate is increased by 8.4% when particle diameter increased from 450 μm to 500 μm (i.e for 12% increase in particle diameter). The erosion rate is continued in increasing rapidly with particle diameter, it reaches to 439% when the particle diameter be 600 μm . This increase in the erosion rate is due to more particle momentum affected on pipe wall is presented since larger particles have more mass than higher momentum energy compared with that for small particles.

4.1.4. Effect of internal pipe diameter

The erosion rate increased with decreasing the pipe internal diameter ID as shown in Fig. (9-d) and given in Table (9). The investigated pipe internal diameter ID are: 203.2, 250, 300, 350 and 406.4 mm. The erosion rate is increased by 28% when internal pipe diameter is decreased by 13.8% ($1.12 \times 10^{-11} \text{ kg/m}^2 \cdot \text{s}$ at 350 mm), and increased by 273% for 50% decreasing in ID ($3.26 \times 10^{-10} \text{ kg/m}^2 \cdot \text{s}$ at 203.2 mm).

The resulted increasing in erosion rate is due to the increase in flow turbulence and the volume fraction of sand particles as the internal pipe diameter decreased. This leads to rise particle collision with pipe wall material and increase erosion.

4.2. Pipe with sudden contraction

Two-phase (water-sand) flow in a horizontal pipe with sudden contraction (0.55 contraction ratio) shown in Figure (1-b) is simulated with the flow conditions given in Table (7). The distribution of

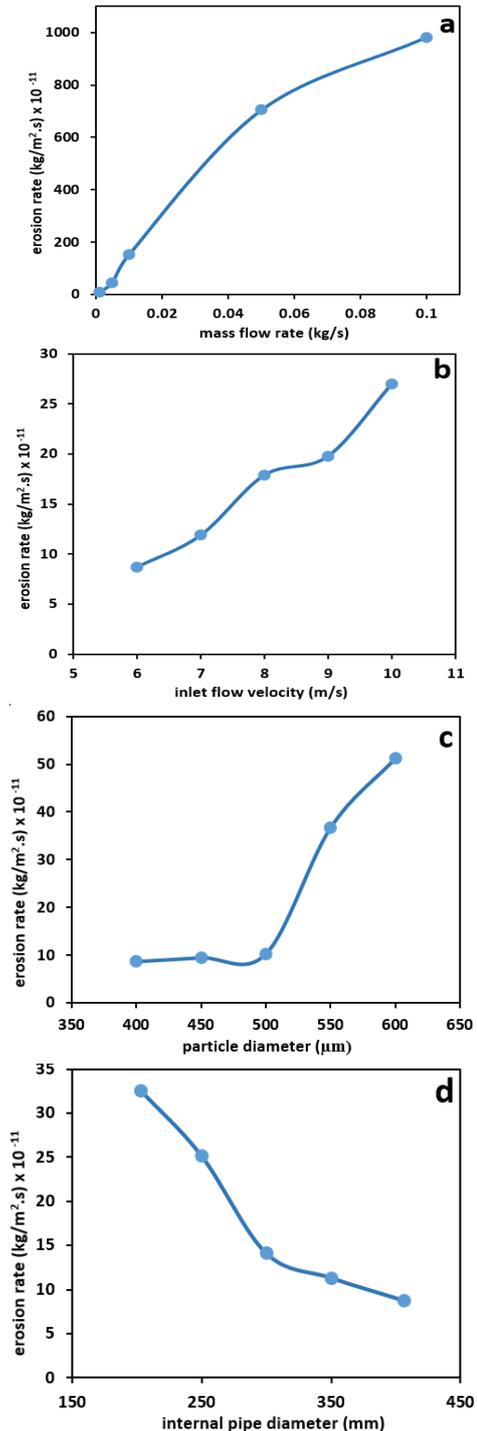


Fig. 9. The relationship between erosion rate and (a) mass flow rate of sand particles (b) inlet flow velocity (c) particle diameter (d) internal pipe diameter

velocity and converging streamlines shown in Fig. (10) illustrates the increasing in flow velocity at the contraction section. The reported pressure reduction at contraction section shown in Fig. (11) is agreed with the expected behaviour according to Euler's equation along streamline. The maximum resulted erosion rate occurs at the step wall contraction area. It is of $(4.116 \times 10^{-8} \text{ kg/m}^2\cdot\text{s})$ due to the direct impaction of sand particles with step wall area as shown in Fig.(12) since vortices region is formed before and after the contraction section.

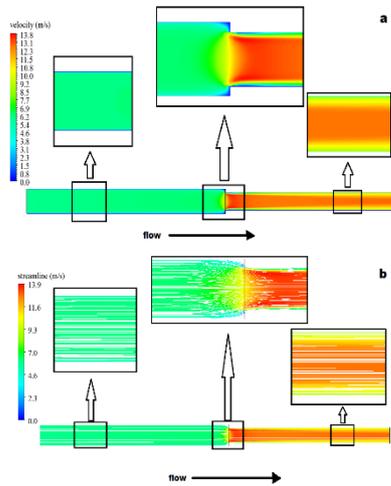


Fig. 10. Distribution of (a) flow velocity (b) streamlines

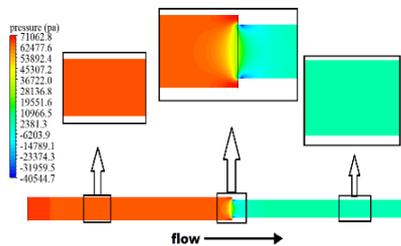


Fig. 11. Distribution of pressure

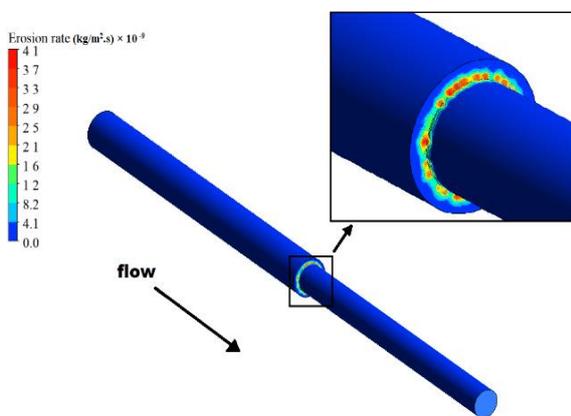


Fig. 12. Erosion behaviour in pipe with sudden contraction case

A parametric study is performed considering the effect of: mass flow rate of sand particles, inlet flow

velocity, particle diameter, internal pipe diameter, contraction coefficient, step wall angle and orientation on erosion behavior as given in Table (10).

4.2.1. Effect of mass flow rate of sand particles

In this work it is found the erosion rate is increased with increasing mass flow rate of sand particles as presented in Fig.(13-a). It was $(4.116 \times 10^{-8} \text{ kg/m}^2\cdot\text{s})$ at (0.001kg/s) and increased by 99 times when mass flow rate is 0.1kg/s as given in Table (10). This is attributed to the increase in particles collisions with step wall material.

4.2.2. Effect of inlet velocity

The erosion rate is increased with increasing inlet flow velocity as shown in Fig. (13-b). It was $(4.11 \times 10^{-8} \text{ kg/m}^2\cdot\text{s})$ at 6 m/s inlet velocity, then increased to $(7.33 \times 10^{-8} \text{ kg/m}^2\cdot\text{s})$ at 7m/s. Then increased to $(1.95 \times 10^{-7} \text{ kg/m}^2\cdot\text{s})$ at 10 m/s. The momentum impact of the particles rises with the increase of particle speed, leading to increase the impact energy and more erosion in step wall material resulted.

4.2.3. The effect of particle size

The erosion rate in pipe with sudden contraction is increased as particle diameter increased till it reaches $500 \mu\text{m}$ then it starts to decrease as presented in Fig.(13-c). At $550 \mu\text{m}$, the erosion rate is increased again. It is found that for the working conditions illustrated in Table (8), the particle diameter of $500 \mu\text{m}$ is form the critical diameter for the erosion in the pipe with sudden contraction. This behaviour is complicated since the flow in pipe contraction is associated with vena contracta phenomena synchronized with solid-liquid flow that results an interaction in the dominated forces for the particles with different diameters with pipe wall [32].

4.2.4. Effect of pipe diameter

Figure (13-d) illustrates an increase in the erosion rate with decreasing internal pipe diameter. It is increased by 70.8% when internal pipe diameter is reduced by 16.7% for the same contraction ratio of (0.5449) . Erosion rate increasing continuously until it reaches 4.117×10^{-7} for 66.7% reduction in pipe diameters. The erosion rate increasing occurs due to the increase in flow turbulence as pipe internal diameter decreased. This leads to rise of particle collision with pipe wall material.

4.2.5. Effect of contraction ratio

The contraction coefficient is an important factor influences the solid particle erosion in the pipe with sudden contraction. The obtained erosion rate is decreased rapidly with the increasing of contraction coefficient as illustrated in Fig. (13-e). The maximum decrease in erosion rate is found to be as $(498.66 \text{ kg/m}^2\cdot\text{s})$ when contraction coefficient is increased from 0.0605 to 0.3784 for the same operating conditions given in Table (8). Also the

decrease in erosion rate is predicted to be (35.76 $\text{kg/m}^2\cdot\text{s}$) as contraction coefficient increased from 0.13623 to 0.3784. The increase in erosion rate resulted from the increase in step wall area so more sand particles collide with it and erosion rate increased.

4.2.6. Effect of step wall angle

The erosion rate is decreased when step wall angle is reduced as seen in Table (10). It is mean that the step wall is contracted gradually instead of suddenly as shown in Fig. (14). Erosion rate decreased by more than 30 times when the contraction wall angle is reduced to 30° (1.24×10^{-9} $\text{kg/m}^2\cdot\text{s}$ at 30° step wall angle). This could be considered as a pointed geometrical solution to reduce erosion in the pipe with contraction. The erosion reduction could be explained with that the particles are collide the step wall area tangentially instead of normally. The particles will lose part of their energy due impaction, leading to reduce erosion. The relation between step wall angle and erosion rate is illustrated in Fig. (13-f).

4.2.7. Effect of orientation

When the pipe orientation is changed from horizontal to vertical, the erosion rate increased by 6.1% as given in Table (10) (test No. 1 is considered as the reference). This increase is due to the effect of gravity, which made the particles accelerate in the direction of the flow, so these particles be abrasive due to their higher momentum effect, and resulted more eroded flow.

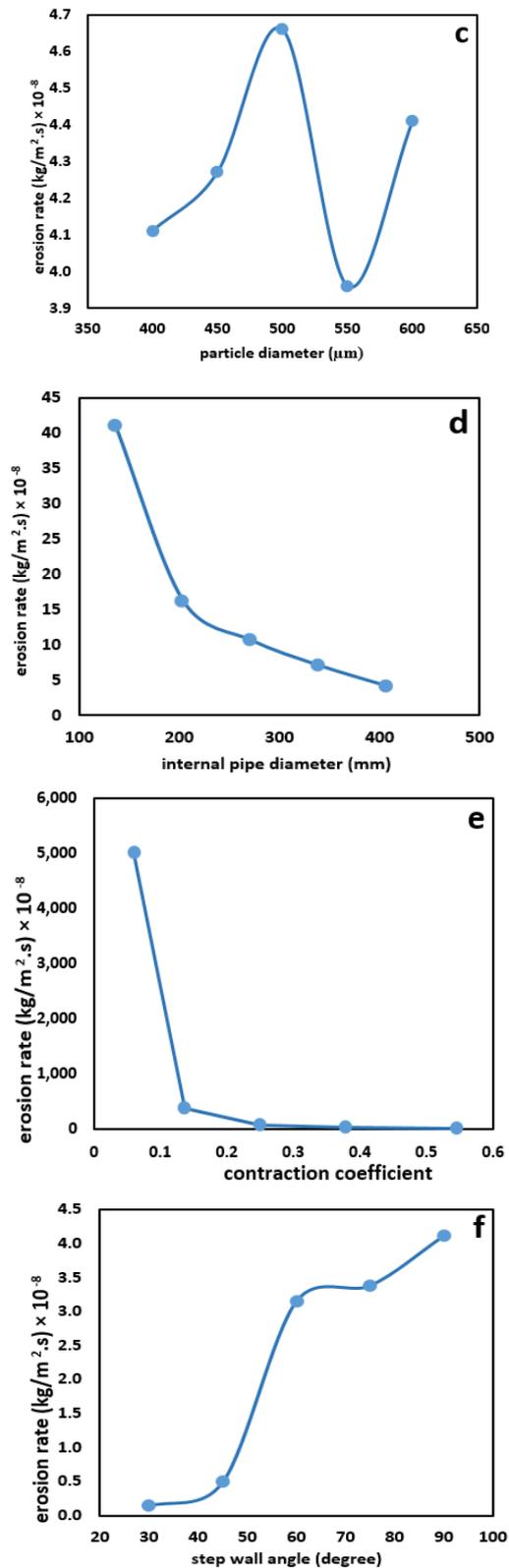
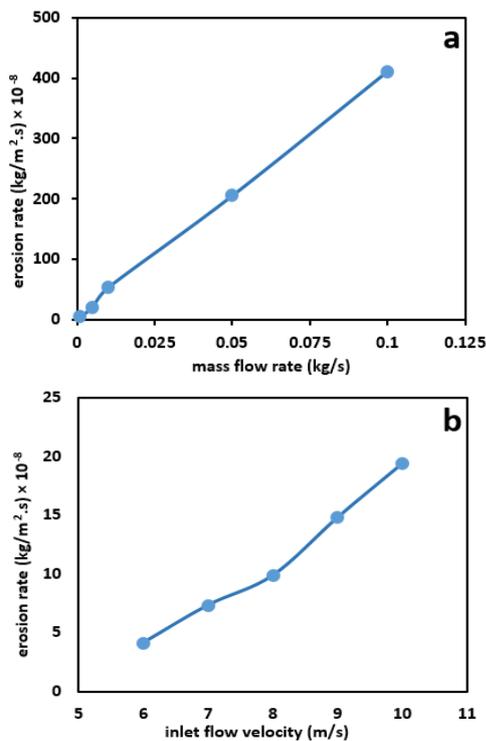


Fig. 13. Variation of erosion rate with: a) mass flow rate of sand particles, b) inlet flow velocity, c) sand particle diameter, d) internal pipe diameter, e) contraction coefficient, f) step wall angle

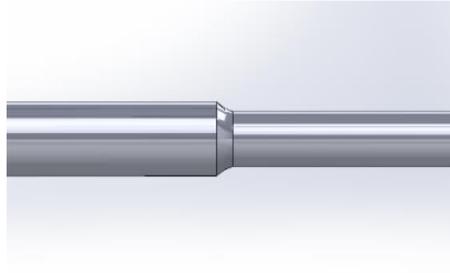


Fig.14. Gradual contraction

Table 10. Effect of different parameters on erosion rate in pipe with sudden contraction case II

No.	Mass flow rate (kg/s)	Inlet velocity (m/sec)	Particle diameter (μm)	Internal pipe diameter (mm)	Contraction coefficient	Step wall angle (deg.)	Orientation	Erosion rate (kg/m ² .s)
1	0.001	6	400	406.4 - 300	0.5449	90°	horizontal	4.12× 10 ⁻⁸
2	0.005	6	400	406.4 - 300	0.5449	90°	horizontal	2.06× 10 ⁻⁷
3	0.01	6	400	406.4 - 300	0.5449	90°	horizontal	5.285× 10 ⁻⁷
4	0.05	6	400	406.4 - 300	0.5449	90°	horizontal	2.06× 10 ⁻⁶
5	0.1	6	400	406.4 - 300	0.5449	90°	horizontal	4.12 × 10 ⁻⁶
6	0.001	7	400	406.4 - 300	0.5449	90°	horizontal	7.33× 10 ⁻⁸
7	0.001	8	400	406.4 - 300	0.5449	90°	horizontal	9.87× 10 ⁻⁸
8	0.001	9	400	406.4 - 300	0.5449	90°	horizontal	1.48 × 10 ⁻⁷
9	0.001	10	400	406.4 - 300	0.5449	90°	horizontal	1.95 × 10 ⁻⁷
10	0.001	6	450	406.4 - 300	0.5449	90°	horizontal	4.28 × 10 ⁻⁸
11	0.001	6	500	406.4 - 300	0.5449	90°	horizontal	4.66× 10 ⁻⁸
12	0.001	6	550	406.4 - 300	0.5449	90°	horizontal	3.96 × 10 ⁻⁸
13	0.001	6	600	406.4 - 300	0.5449	90°	horizontal	4.41× 10 ⁻⁸
14	0.001	6	400	338.66 - 250	0.5449	90°	horizontal	7.03× 10 ⁻⁸
15	0.001	6	400	271 - 200	0.5449	90°	horizontal	1.06× 10 ⁻⁷
16	0.001	6	400	203.2-150	0.5449	90°	horizontal	1.63× 10 ⁻⁷
17	0.001	6	400	135.46-100	0.5449	90°	horizontal	4.12× 10 ⁻⁷
18	0.001	6	400	406.4 - 250	0.3784	90°	horizontal	2.34× 10 ⁻⁷
19	0.001	6	400	406.4 -203.2	0.25	90°	horizontal	6.38× 10 ⁻⁷
20	0.001	6	400	406.4 - 150	0.13623	90°	horizontal	3.81 × 10 ⁻⁶
21	0.001	6	400	406.4 - 100	0.0605	90°	horizontal	5.01 × 10 ⁻⁵
22	0.001	6	400	406.4 - 300	0.5449	75°	horizontal	3.38 × 10 ⁻⁸
23	0.001	6	400	406.4 - 300	0.5449	60°	horizontal	3.15× 10 ⁻⁸
24	0.001	6	400	406.4 - 300	0.5449	45°	horizontal	4.94 × 10 ⁻⁹
25	0.001	6	400	406.4 - 300	0.5449	30°	horizontal	1.42× 10 ⁻⁹
26	0.001	6	400	406.4 - 300	0.5449	90°	vertical	4.37 × 10 ⁻⁸

5. CONCLUSIONS

According to the two-way coupled with Eulerian-Lagrangian approach and the coupled erosion model with constant coefficient of restitution. A 3-D numerical analysis was proposed to investigate the erosion of two phase (sand-water) turbulent flow in two piping geometries: straight

pipe and pipe with sudden contraction. The effect of solid particle mass flow rate, inlet velocity, pipe diameter, particle size, contraction ratio, step wall angle and orientation are examined. The conclusions could be drawn are:

- (1) The erosion behavior distributed homogenously in the straight pipe case. But, in the pipe with

sudden contraction the most erosive area is at the step wall.

- (2) The erosion rate increased with increasing solid particles concentration, increasing inlet velocity and decreasing pipe diameter for both straight pipe, and pipe with contraction section.
- (3) The erosion behavior is not conserved with the effect of particle size in the present considered pipe geometries. For the straight pipe, the erosion rate increased with increasing particle size. While, for pipe with sudden contraction, the erosion rate increased with increasing particle size till particle critical diameter of 500 μm . Then erosion rate is decreased, and start to increase again after 550 μm particle diameter.
- (4) Increasing the contraction ratio of the pipe with sudden contraction decreases the erosion rate.
- (5) The erosion rate in the pipe with a contraction is highly influenced by the angle of step wall. The erosion rate decreased by 30 times with decreasing step wall angle to 30° compared with that for 90°. So, changing the step wall angle could be considered as geometrical solution to reduce erosion rate in the pipe with contraction.

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